



Thermal energy storage implementation using phase change materials in a solar cooling and refrigeration applications

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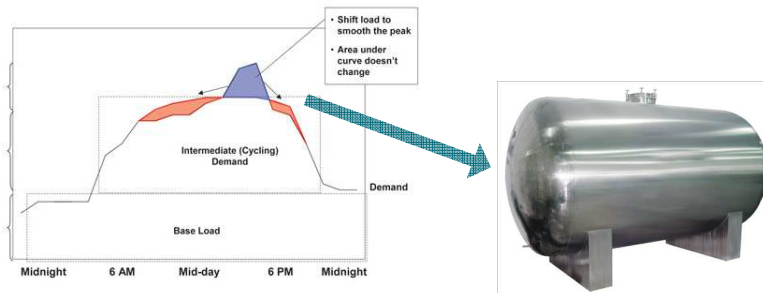
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- Nowadays, solar cooling and refrigeration technology have become vital for both human comfort since solar energy is the cheapest and most extensively available renewable energy
- In solar vapor absorption systems, the energy received from the solar collector is given as heat input to the generator; hence it has to assure a constant heat input to the absorption chiller during all the process



Introduction

- Here the main disadvantage of this energy resource is the mismatch between the energy supply and the energy demand
- Therefore, when energy is available but cannot be given to the process, thermal energy storage (TES) may become an important issue



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Objective

- To select and to test different phase change materials (PCM) candidates in lab scale
- To compare the PCM selected at pilot plant scale in a real high temperature system

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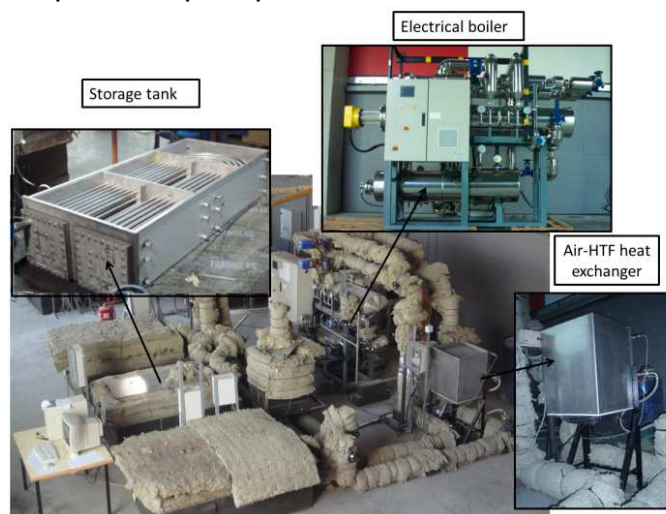
Materials and methodology

- Selection of the PCM
 - Storage temperature 140 – 200 °C
 - Heat of fusion > 150 kJ/kg

| Material | Experimental phase change temperature [°C] | Experimental phase change enthalpy [kJ/kg] |
|-----------------------|--|--|
| Salicylic acid | 159.1 (m) / 111.3 (s) | 161.5 (m) / 109.4 (s) |
| Benzanilide | 163.6 (m) / 136.1 (s) | 138.9 (m) / 129.4 (s) |
| D-mannitol | 166.8 (m) / 117 (s) | 260.8 (m) / 214.4 (s) |
| Hydroquinone | 172.5 (m) / 159.5 (s) | 235.2 (m) / 178.7 (s) |
| Potassium thiocyanate | 176.6 (m) / 156.9 (s) | 114.4 (m) / 112.5 (s) |

Materials and methodology

- High temperature pilot plant



- High temperature pilot plant - boiler



| | Value |
|-----------------------------------|---------|
| Electrical power [kW] | 24 |
| Thermal heating power [kW] | 20 |
| HTF flow rate [m ³ /h] | 0.3 - 3 |
| Maximum pressure of work [bar] | 15 |
| Maximum temperature of work [°C] | 400 |

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- High temperature pilot plant – air heat exchanger



| | Value |
|-----------------------------------|-------------|
| Thermal cooling power [kW] | 20 |
| Air flow rate [m ³ /h] | 1800 |
| Air inlet temperature [°C] | ambient |
| Exterior dimensions [mm] | 700x540x440 |

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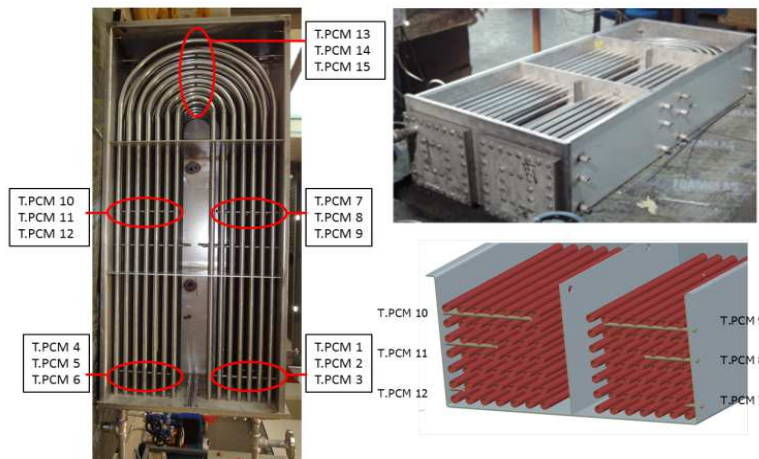
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- High temperature pilot plant - tank



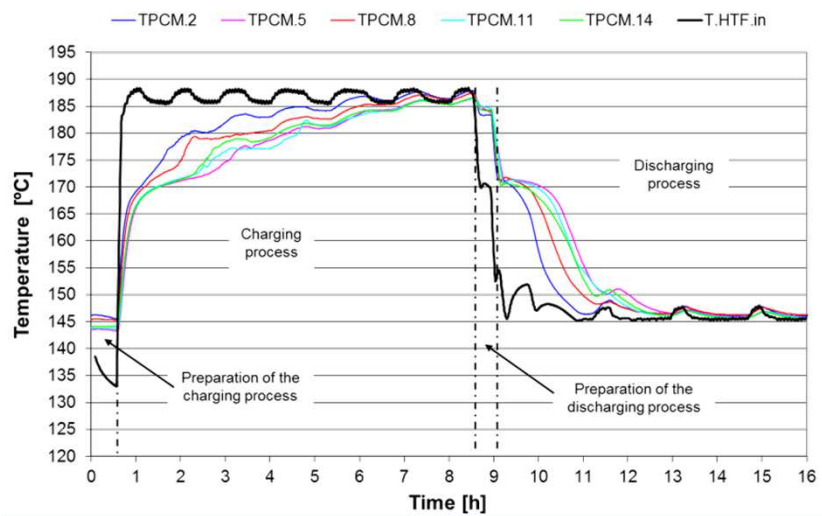
| | Value |
|---|-------|
| Storage tank width [m] | 0.527 |
| Storage tank height [m] | 0.273 |
| Storage tank depth [m] | 1.273 |
| Number of HTF tubes [-] | 49 |
| HTF pipes average length [m] | 2.90 |
| Heat transfer surface [m ²] | 6.568 |
| Total d-mannitol mass [kg] | 160 |

- High temperature pilot plant - tank

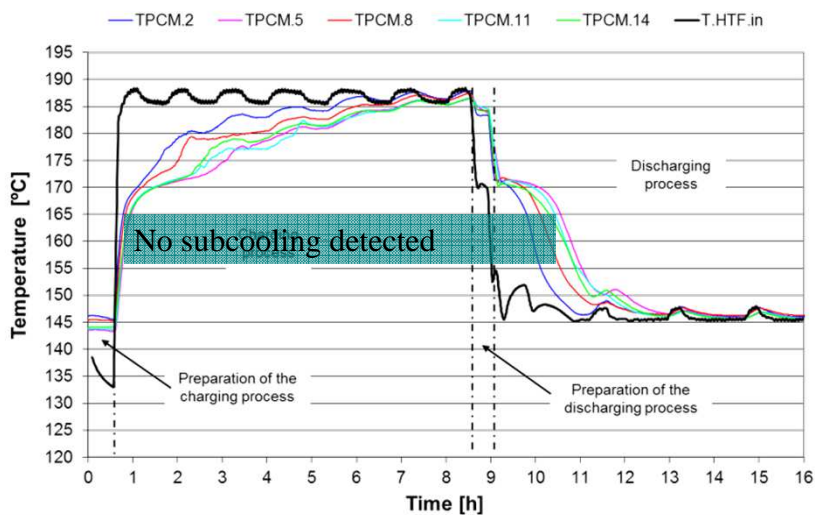


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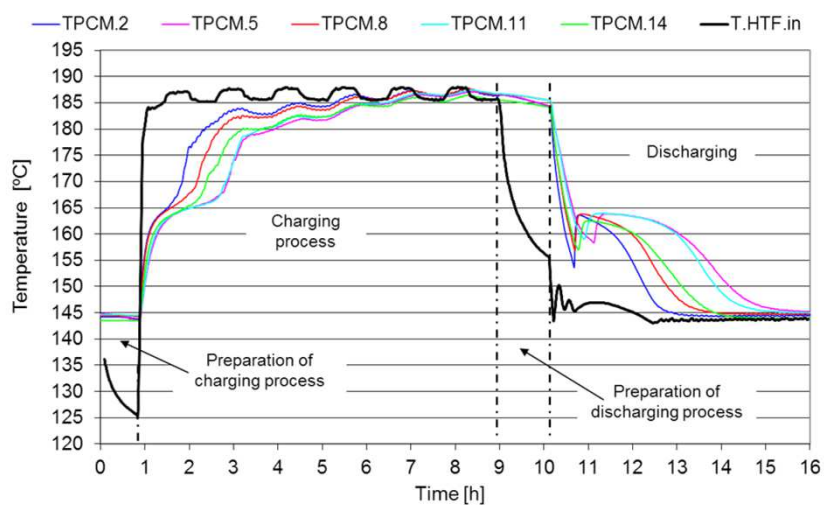
- Hydroquinone – temperature profile



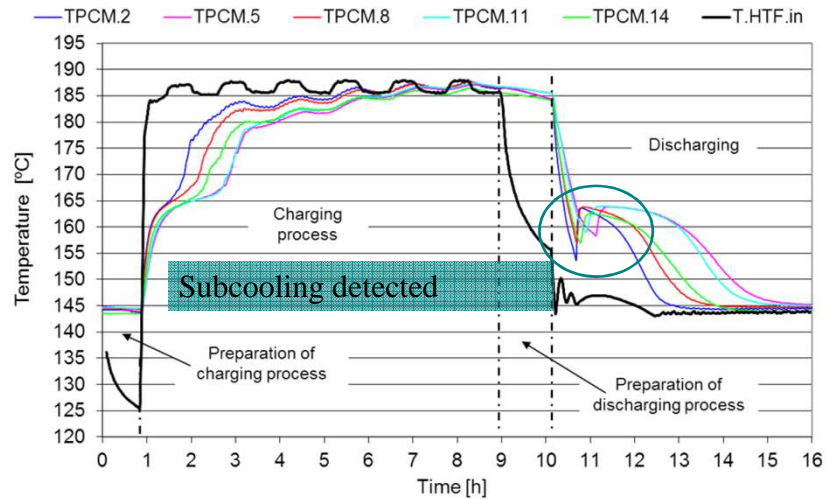
• Hydroquinone – temperature profile



• D-mannitol – temperature profile



- D-mannitol – temperature profile

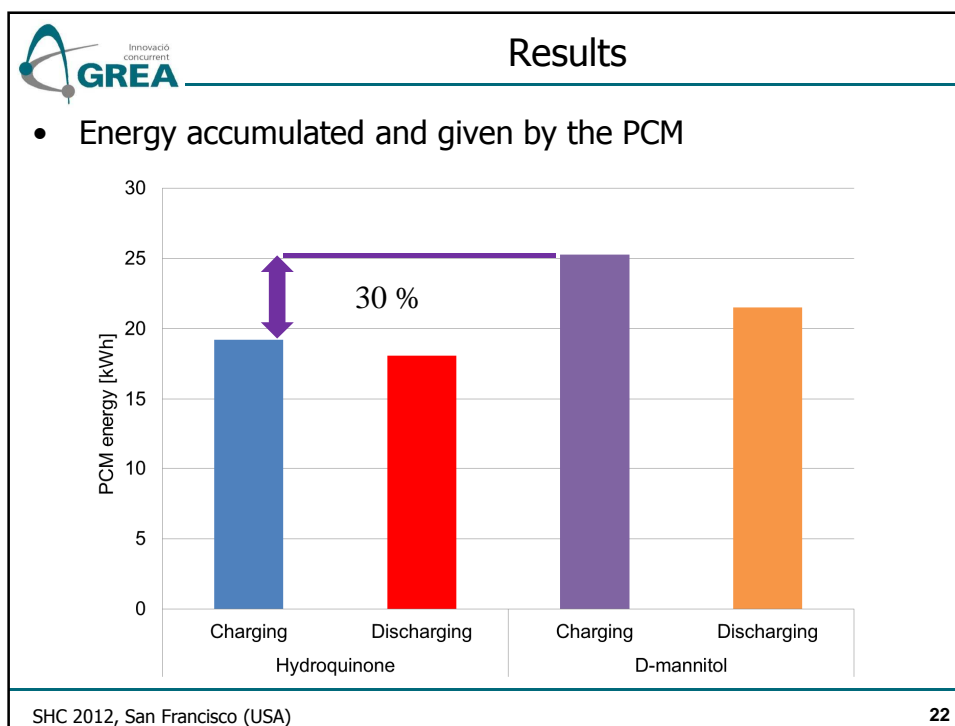
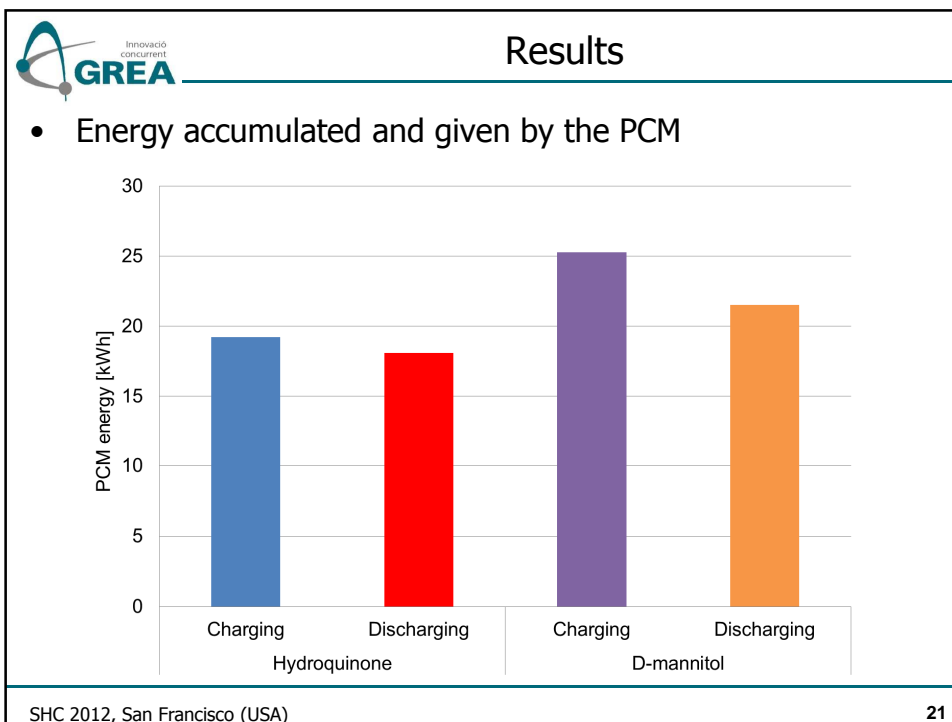


- Energy balance in the storage tank

$$- Q_{HTF} = Q_{PCM} + Q_{tank} + Q_{loss} + Q_{acc HTF} + Q_{insulation}$$

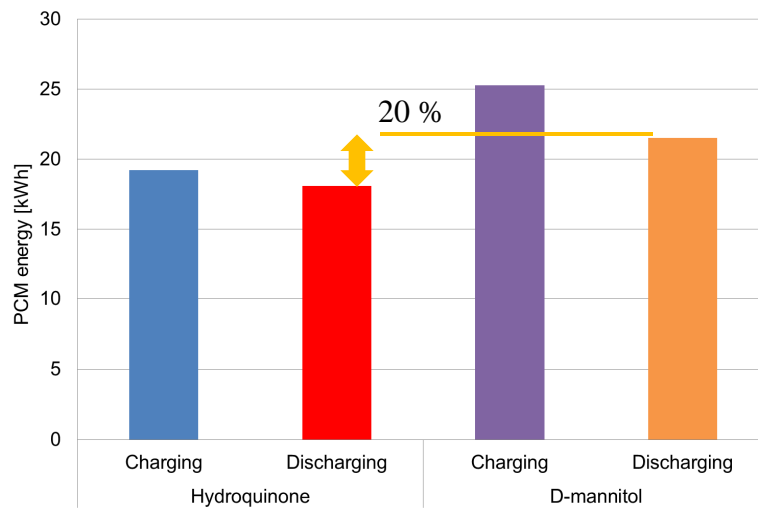
$$- \varepsilon_{cha} = \frac{Q_{PCM}}{Q_{HTF}} \quad \varepsilon_{dis} = \frac{Q_{HTF}}{Q_{PCM} + Q_{steel}}$$

| | Hydroquinone | | D-mannitol | |
|--------------------------|--------------|-------------|------------|-------------|
| | Charging | Discharging | Charging | Discharging |
| Time [min] | 476 | 362 | 486 | 354 |
| ΔE_{HTF} [kWh] | 21.5 | 17.9 | 27.7 | 21.4 |
| ΔE_{PCM} [kWh] | 19.2 | 18.1 | 25.3 | 21.5 |
| ΔE_{loss} [kWh] | 1.4 | 1.2 | 1.3 | 0.8 |
| ΔE_{steel} [kWh] | 0.8 | 0.5 | 0.9 | 0.5 |
| ε [-] | 0.9 | 0.96 | 0.91 | 0.97 |



Results

- Energy accumulated and given by the PCM



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Conclusions

- A high temperature pilot plant with TES system based on shell-and-tubes heat exchanger were designed and built at the University of Lleida
- Literature and DSC research of some PCM candidates for solar cooling applications were done
- Hydroquinone and d-mannitol were the PCM selected to test them at pilot plant scale
- Different charging and discharging experiments with different flow rates and HTF temperatures were performed

Conclusions

- For both PCM, no hysteresis was detected, and even though hydroquinone presented subcooling in the DSC, it did almost not appear in pilot plant scale, however, when d-mannitol was used big subcooling was detected
- For the same boundary conditions, the energy stored by d-mannitol was higher than that for hydroquinone
- The enhancement was about 30% and 20% during the charging and the discharging processes even though the enhancement of the latent heat was only 10 and 16%, respectively

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- To all co-authors of this work



Thank you for your attention

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