



Refrigeration technology about solar adsorption, absorption and Photovoltaic

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March, 27th,2015

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Contents







Solar Heating Adsorption Refrigeration 1.1 Working principle

Working principle :

Energy is transferred through phase-change processes (evaporation heat)



Solar adsorption

Working Pairs

activated carbon -methanol; molecular sieve -water; silica gel -water; activated carbon -ammonia and so on.

form : Single bed 、 multiple-bed





The most important research work of solar heating adsorption refrigeration is: How do we improve the efficiency?

There are two ways adopted to improve the efficiency of solar heating adsorption.

a. Enhancing heat transfer

b. Enhancing mass transfer





1.2 solar heating adsorption refrigeration——Enhancing heat transfer 1.2.1 Optimization of adsorption bed

Designing a fin-tube adsorption collecting bed



Sectional view

Material: pure Aluminum or
Aluminium alloyOuter tube diameter:90mmInter tube diameter:27.4mmFin angle:60°Disconnect width
of the inner tube:2mmFin length:15mmPipe wall thickness:1.2mm

Advantages:

- 1. enhancing heat transfer
- 2.improving adsorption tube resistance3. improving sealing performance





1.2.1 Optimization of adsorption bed



Finned tube Activated carbon adsorbent





1.2.2 Optimization of condenser



Outer material: pure Aluminum Inter material: pure copper Fin outer diameter: 32.5mm Fin inter diameter: 15.5mm Fin spacing: 2.5mm

Advantages:

- 1. Increasing heat exchange area
- 2. enhancing heat transfer
- 3. improving cooling uniformity







1.2.3 Optimization of evaporator



Advantages:

- 1. Increasing contact area
- 2. enhancing ice making rate
- 3. Alleviating super cooling phenomenon

Parameter Shell size: 350mm*350mm*100mm Effective evaporation area: 0.46m² Volume: 7.8L







1.2.4 Parameters of adsorption bed



1 glass cover 2 finned adsorption tube 3 draft tube 4 Thermal insulating layer Structure diagram of adsorption bed

| Size(L*W*H) | 1560mm*1320m m*150mm |
|-----------------------------|-------------------------|
| absorbing area | 1.1m ² |
| Quality of activated carbon | 29kg |
| Quality of adsorption tube | 29kg |
| Adsorption bed area | 10.8m ² |





1.2 solar heating adsorption refrigeration—Enhancing heat transfer 1.2.5 Experimental platform



Structure diagram



Photos of the system





1.2 solar heating adsorption refrigeration—Enhancing heat transfer 1.2.7 Ice making



Ice making process







Compared with the Solar ice maker developed in 2002







1.2 solar heating adsorption refrigeration—Enhancing heat transfer 1.2.8 Test results

The highest adesorption temperature and the time of closing valve (cloudless day)

| | March 19 | March 23 | March 24 |
|-------------------------|--------------|------------------------|--------------|
| Time of closing valve | 15:00 | 14:40 | 15:30 |
| Radiation (MJ) | 20.5 | 18.2 | 18.2 |
| Highest temperature(°C) | 91.5 | 90.1 | 83.5 |
| Time | 13:45 | 14:20 | 15:15 |
| COP _{solar} | <u>0.122</u> | <u>0.129</u> | <u>0.112</u> |
| Note | Cloudless | Cloudless before 14:40 | Cloudless |

the highest adesorption temperature and the time of closing valve (cloudy day)

| | March 20 | March 21 | March 22 |
|-------------------------|--------------|--------------|--------------|
| Time of closing valve | 15:00 | 15:00 | 15:00 |
| Radiation (MJ) | 21.5 | 20.8 | 15.0 |
| Highest temperature(°C) | 93.4 | 89.8 | 81.5 |
| Time | 14:22 | 14:15 | 12:35 |
| COP _{solar} | <u>0.094</u> | <u>0.094</u> | <u>0.079</u> |
| Note | cloudy day | cloudy day | cloudy day |





1.2 solar heating adsorption refrigeration—Enhancing heat transfe **1.2.9 Accomplishments**

National Fund:

The mass and energy transmission and coupling energy research about solar heating adsorption refrigeration driven by medium temperature energy based on trough concentrating , 51366014

patent :

A fin tube type solar adsorption refrigeration system, CN 202209810 U





1.3.1 We have found Some problems during the experiment:

a. The refrigerant gas mass transfer resistance was very high. Therefore, the desorption time was very long in desorbing process and the outer wall of pipeline was very hot as well as the number of vacuum pressure was high.

b. The desorption process was not complete. Some refrigerant heated in collector can not flow into condenser on time. Subsequently, they absorbed in absorption bed at low temperature.

c. methanol adsorption refrigerant did not vaporize indirectly but atomized at first and then vaporized slowly.





1.3.2 Analysis and solution

The reason is that desorbed gas blocked in mass transfer process, which resulted in refrigerant circulating rate and energy utilizing rate were not improved in refrigerating process.

To solve the problem, the pipeline pump should be installed in mass transfer pipeline to accelerate the adsorption gas transferring and refrigerant desorbing in absorption bed.





1.3.3 Enhancing mass transfer assisted with Photovoltaic

Considering that working time is synchronous among pipeline pump, solar collector and adsorption bed. The Photovoltaic will be adopted to provide power for pipeline pump.

Refrigeration efficiency and energy utilization rate can be improved. Furthermore, comprehensive utilization performance of solar photovoltaic and solar Thermal system can be enhanced.





1.3.4 Photovoltaic together with strengthen mass transfer and solar adsorption refrigeration system



- 1. The finned tube collector/adsorption bed
- 2. Glass cover
- 3. The thermal insulation material
- 4. Solar panels
- 5. The controller
- 6. Pipeline pump
- 7. Check valve
- 8. The condenser
- 9. The evaporator
- 10. Heat insulation water tank
- 11. The pressure gauge





1.3.4 Photovoltaic together with strengthen mass transfer and solar adsorption refrigeration system



Dc pipe pump (micro vacuum pump)

Photovoltaic strengthen adsorption refrigeration real figure

The solar panels





1.3.5 System performance contrast test results in the two modes of mass transfer

The refrigeration system performance under the mode of natural mass transfer

| Drojact | September 5 | 5 September 8 | September | September | September |
|---|-------------|---------------|-----------|-----------|-----------|
| Floject | | | 11 | 14 | 17 |
| The heating time (h) | 8.5 | 8.0 | 7.5 | 7.0 | 6.5 |
| Receive the total radiation (${ m MJ}$) | 19.278 | 18.144 | 17.010 | 15.876 | 14.742 |
| The amount of ice/cold wate (kg) | 4.8/2.2 | 3.7/4.3 | 3.0/4.0 | 2.3/4.7 | 2.0/5.0 |
| Direct refrigerating capacity (MJ) | 2.201 | 1.809 | 1.602 | 1.180 | 1.023 |
| СОР | 0.114 | 0.100 | 0.094 | 0.074 | 0.069 |

The refrigeration system performance under the mode of strengthen mass transfer

| Project | September 6 | September 7 | September 12 | September 13 | September 16 |
|---|-------------|-------------|--------------|--------------|--------------|
| The heating time (h) | 8.5 | 8.0 | 7.5 | 7.0 | 6.5 |
| Receive the total radiation (${ m MJ}$) | 19.278 | 18.144 | 17.010 | 15.876 | 14.742 |
| The amount of ice/cold wate (kg) | 7.0/0 | 5.8/2.2 | 5.0/2.0 | 4.2/2.8 | 2.8/4.2 |
| Direct refrigerating capacity | 2.896 | 2.609 | 2.019 | 1.856 | 1.600 |
| COP | 0.150 | 0.144 | 0.119 | 0.116 | 0.109 |
| | | | | | |



1.3.6 Interpretation of results

Under the same conditions the COP was higher than 58.0%, 56.8%, 26.6%, 44.0% respectively and ranged from 58.0%, to 44.5% in the average.

It is clear that this system under the mode of strengthening mass transfer has a high cooling efficiency, and the cooling performance was more stable, Therefore, strengthening mass transfer has obvious advantages than the mode of the natural mass transfer.



System COP contrast under the mode of natural/strengthen mass transfer





1.3.7 Adsorbent bed temperature changes in two modes



The adsorption heat under enhancing mass transfer was significantly higher than it under the natural mass transfer in the adsorption stage.



1.3.8 the cold water / ice temperature changes in two modes



Mass transfer enhancement

Natural mass transfer

With the method of enhancing mass transfer , ice condensation rate was more faster !





1.3 solar heating adsorption refrigeration—Enhancing mass transfer **1.3.9 Pressure changes in the system at two modes**



The system vacuum gauge changes over time under enhancing mass transfer Vacuum gauge changes over time under natural mass transfer

With pipeline pump, we can reduce the time of depriving vacuum, and maintain pressure stable between the condenser and the evaporator.







With the aid of the pipeline pump, water and ice temperature can effectively reduce in the evaporator and the entire adsorption refrigerator performance is effectively improved .





2 solar absorption refrigeration

Solar absorption refrigeration is based on solar energy as a driving source, thus we can get cold by relative changes occur of the refrigerant and absorbent concentration.

Absorption refrigeration technology is a mature technology ,which has entered the stage of commercial applications, mainly using LiBr/H₂O absorption chiller.





- 2 solar absorption refrigeration2.1 Working principle
- Working principle :

Energy is transferred through phasechange processes (evaporation heat)







Dynamic principle diagram of absorption chiller





2 Solar absorption chilling

2.2 LiBr/H₂O absorption chilling







2.2 Single-effect LiBr/H₂O absorption chilling 2.2.1 23kW system construction

| 前式太阳能集热阵列 | |
|--|-----|
| Frage< | √机组 |

Pictures of refrigeration system

Parameters of PTC

| 项目 | 数值或说明 |
|----------|----------------------------|
| PTC 开口面积 | 56 m^2 |
| 轴向 | 南北向 ($\psi = 0^{\circ}$) |
| 集热管长度 | 26 m |
| 开口宽度 | 2.5 m |
| 焦距 | 1.1 m |
| 工质 | 水 |
| 行数 | 2 |
| 集热管的内管直径 | 4 cm |
| 集热管玻璃外径 | 11cm |

System parameters

| 项目 | 数值 |
|--------|------------------------------|
| 型号 | TX-23 |
| 冷冻水出口 | 10.0 °C |
| 空气温度 | 36.0 °C |
| 热水进口温度 | 90.0 °C |
| 制冷机容量 | 23 kW |
| 冷冻水流量 | $4.0 \text{ m}^{3}/\text{h}$ |
| 热水流量 | 5.7 m ³ /h |
| 机组重量 | 1200 kg |

Parameters of PTC

| parameter | value | unit |
|--------------------------|-------------|----------------|
| Collector area | 56 | m ² |
| Rotation axial direction | North-south | - |
| Absorber tube length | 26 | m |
| Concentrator width | 2.5 | m |
| Focal length(f) | 1.1 | m |
| Operating temperature | 50-93 | °C |
| PTC row number | 2 | _ |
| Diameter of inner tube | 4 | cm |
| Diameter of glass cover | 11 | cm |



PTC arrays





Parameters of cooling tower

| parameter | value | unit |
|----------------------|--------|-------|
| MODEL | BLT-10 | - |
| Air volume | 10.5 | km³/h |
| Cooling water volume | 10 | m³/h |
| Motor power | 0.75 | kW |
| Net weight | 165 | kg |
| Operating weight | 330 | kg |





Par all and

Parameters of refrigerating unit

| parameter | value | unit |
|----------------------------------|---------------|------|
| MODEL | TX-23 | - |
| Cooling water outlet temperature | 10.0 | °C |
| Hot water inlet temperature | 90.0 | °C |
| Power consumption | 2.3 | kW |
| Refrigeration capacity | 23 | kW |
| Flow of cooling water | 3.24(0.9kg/s) | m³/h |
| Flow of hot water | 4.9(1.36kg/s) | m³/h |
| Unit weight | 1200 | kg |
| | | |

Parameters of fan-coil EKCW800KT

| parameter | value | unit |
|------------------|-----------|------|
| MODEL | EKCW800KT | - |
| Н | 1360 | m³/h |
| Μ | 1210 | m³/h |
| L | 1100 | m³/h |
| Cooling capacity | 7200 | W |
| Heating capacity | 10800 | W |
| Input power | 130 | W |



2.2 Double-effect LiBr/H₂O absorption chilling

2.1.1 Experimental results





Temperatures of heating, refrigerating and cooling outputs







Inlet and outlet temperatures of generator, evaporator and condenser



Temperature variation of refrigeration terminal (a meeting room)

T1–T7 are temperatures of different positions in the room, meeting room volume : 279m³ (testing time : 2014-03-02)

Room temperature dropped from 19°C to 13°C, COP was 0.35-0.71



3 Solar energy photovoltaic refrigeration 3.1 The working principle

• Working principle :

Through the panel light into electricity, and then through the controller, inverter, battery

driven refrigerators work, etc.







3.2 Solar energy photovoltaic fridge

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3.2.1 Photovoltaic fridge working principle and experiment platform







3.2 Solar energy photovoltaic fridge

3.2.2 Photovoltaic fridge experimental results

| Date | 2013.08.30 | 2013.09.15 | 2014.05.28 | 2014.05.30 |
|--|------------|------------|------------|------------|
| Receive the total radiation (MJ) | 5.37 | 12.19 | 11.3 | 13.79 |
| The fridge minimum temperature (°C) | -9.7 | -15.5 | -16.0 | -17.7 |
| lce-making capacity (kg) | 1.58 | 3 | 6 | 7 |
| СОР | 0.15 | 0.12 | 0.25 | 0.24 |



3.2 Solar energy photovoltaic fridge

3.2.3 Photovoltaic fridge performance analysis



Solar energy fridge system performance test under the condition of suny day

The freezer and fridge temperature dropped to 0 °C, 5 °C, respectively whithin 60 min, 18 min, provided power by standing alone solar panels, battery voltage added 1.6 V in the process of experiment







Solar energy fridge system performance test under the condition of cloudy day

The freezer and fridge temperature dropped to 0 and 5 °C, respectively whithin 50 min, 130 min, the storage battery and solar panels alternating provide power to the system in the experiments, battery voltage droped 1.6 V in the process of experiment







Solar energy fridge system performance test under the condition of overcast day

The fridge is provided power by the storage battery ,the minimum temperature of the freezer was - 22 °C, freezer temperature was cyclical changed within 0 to 6 °C, storage battery voltage drop 1.9 V, the fridge operation rate was 32%



3.3 Solar energy photovoltaic air-condition

3.3.1 Photovoltaic air-condition system main components



The air-condition

The storage battery

ERSITY





3.3 Solar Energy Photovoltaic Air Conditioner 3.3.2 Parameters of photovoltaic air conditioning system



| part | Parameter name | Value |
|-----------------------------|---------------------------|-------------|
| Solar cell array | Rated power | 2.65kw |
| Controller | Rated voltage | 48V |
| | Maximum current | 60A |
| Inverter | Rated voltage | 48V |
| | Rated power | 3kW |
| Battery | Rated voltage | 48V |
| | Rated power | 130Ah |
| Inverter Air Conditioner | Refrigeration input power | 0.1—1.4kW |
| | Heating input power | 0.19—1.57kW |

Solar energy photovoltaic air conditioning office

Parameters of solar energy photovoltaic air conditioning system





3.3 Solar Energy Photovoltaic Air Conditioner 3.3.2 Performance analysis of photovoltaic air conditioner for energy supply model



The drop graph of cooling Air temperature





3.3 Solar Energy Photovoltaic Air Conditioner 3.3.2 Performance analysis of photovoltaic air conditioner for energy supply model



The rise graph of heating Air temperature





3.3 Solar Energy Photovoltaic Air Conditioner

3.3.3 Photovoltaic air conditioner Operation Conditions



| Time of only batteries supply energy | | | | |
|---|----------|--|--|--|
| Maximum power at the thermal mode | 7 hours | | | |
| Maximum power at the refrigeration mode | 9 hours | | | |
| Automatic Mode | 13 hours | | | |

System voltage parameter change

System operation time



3.3.4 The result analysis of combined power supply at the mode of

PV modules and battery p_{25} pov r_{1} ϵ_{Pa}



The maximum charging current of the battery was 26.5A, Total charging of battery during the operation was 58Ah



PV power and air conditioning power

The total output of electrical energy was bigger than the air conditioning total electricity consumption on day time , highest generated output 2.2kW,and the ai conditioning maximum power was 0.8kW



3.3 Solar Energy Photovoltaic Air Conditioner 3.3.5 The result analysis of power supply at the mode of batterypowered Current of Battery ----Indoor temperature Voltage of Battery Outdoor temperature Current of Battery/A Voltage of Battery/V 21 Temperature/C 18 15 12 50 ~~~~~~~~~~~ 12:31 15:31 17:01 11:01 14.01 Time 11:01 12:31 14:01 15:31 17:01

Time

Indoor and outdoor environment temperature variation figure

The time operation for the Air conditioner was 8:30-12:00 and 14:00-18:00. it was found that the average air temperature differences between indoor and outdoor was 10.5°C during the operation periods.

Battery current and voltage variation figure

Battery Max discharging current was 16.3A , battery minimum voltage was 49.8V







3.4 solar photovoltaic ice making and ice storage air conditioning

Ice storage is widely used in central air conditioning system of large buildings for its low cost and mature technology because it can alleviate the pressure of electricity using peak and save electric charge

Set up a experimental platform



Photo of ice maker







3.4 solar photovoltaic ice making and ice storage air conditioning **3.4.1** Experimental results

| Ice (kg/d) | 23.2 |
|--|------|
| Power consumption (kW-h/d) | 9.50 |
| Ice making efficiency | 0.40 |
| Cold exchanger efficiency | 0.70 |
| Comprehensive efficiency | 0.28 |
| Ice temperature (°C) | -5 |
| Ice storage tank temperature (°C) | -2 |
| Refrigerant outlet temperature (°C) | 2 |
| Air conditioner outlet temperatre (°C) | 15 |
| Refrigerating capacity unit PV (W/m^2) | 310 |

The air conditioning system efficiency was 0.28 which is close to the single effect LiBr/H₂O absorption system







Output power changes with irradiance and its stability is very poor so the coupling performance between PV and energy using units will be given the priority of research work in future.

Current changing with irradiance is the main reason for the instability of output power







The consumed Power was 380W by ice maker which is always stable in ice making Time consuming was 10min and ice quality was 0.32kg in every ice making process.



process



4 Summary

4.1 Solar heating adsorption refrigeration

- a. The refrigeration efficiency can be improved by 50% with enhancing the mass transfer achieved by pipeline pump. At the same time, refrigerating cycle can be shortened.
 - b. Green refrigeration will come true when photovoltaic is used to drive pipeline pump to enhance refrigerant mass transfer.





4 Summary

4.2 Solar heating absorption refrigeration

a. Driven by trough concentration heating system, 23kW Double LiBr/H₂O absorption refrigeration coefficient can reach about 0.37 at a running stable system .

b. The temperature of $50m^2$ meeting room can drop from 19 degree down to 13 degree within 2 hours and remaining stable when it is cooled by 23kW Double LiBr/H₂O absorption refrigeration driven with trough concentration heating system.





4 Summary

4.3 Photovoltaic refrigeration

a. The development of PV refrigeration is depending on the cost and technology of energy storage, the main problem is the energy storage, therefore it should be changed to a PV refrigeration.

b. Ice storage technology has a huge advantages for replacement the batteries.





